



# Using FOG and Foodwaste to Increase Methane Production

**NACWA 2011**

**National Pretreatment & Pollution  
Prevention Workshop**

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**HDR**

# Terms

- **Co-digestion** –two or more inputs to digester
- **FOG** - **FATS, OILS, and GREASE**
- **IKG** - **Inedible Kitchen Grease or trap grease**
- **Brown Grease** - trap grease and sewer grease
- **Yellow Grease** - Used cooking oil from restaurants
- **SSO** –source separated organic (preconsumer) such as fruit and vegetable scraps
- **CHP** – Combined Heat and Power

# Introduction and Overview

Why accept FOG and Food waste?

FOG & Foodwaste will increase digester biogas production (more methane).



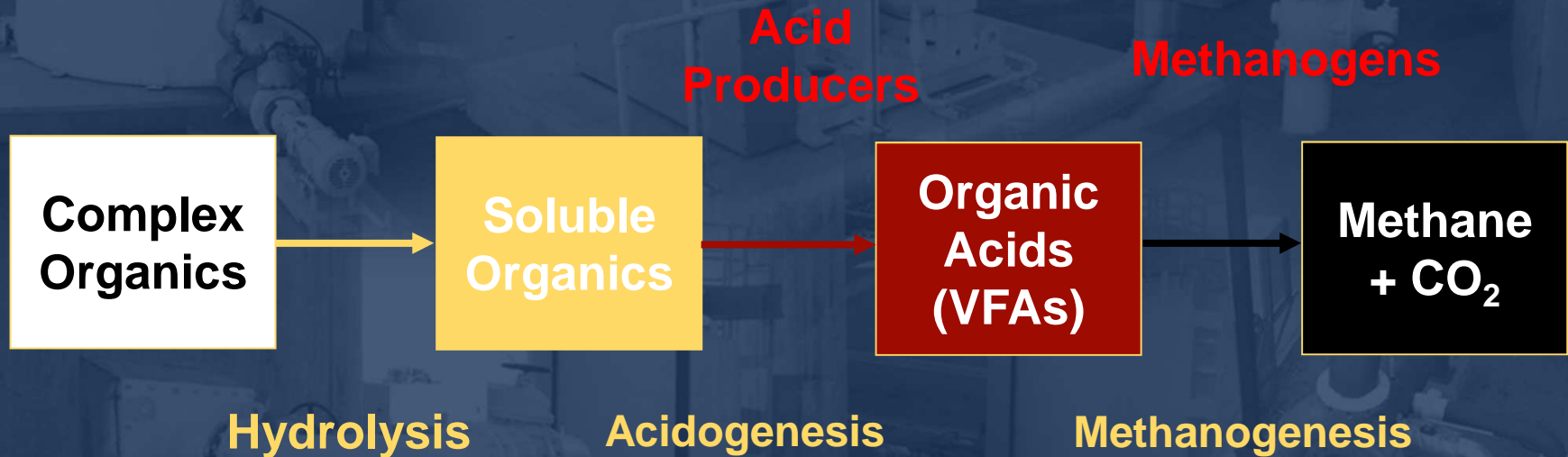


# Key Points

- Fats, Oils, and Greases (FOG) are very high energy feedstock to digesters.
- Separating FOG can eliminate problems in sewer collection systems.
- SSO food waste also a high energy feedstock.
- Utilize excess digester capacity and generate more biogas.

# Anaerobic Digestion Process

## Anaerobic digestion (simplified)



# Biogas Production

	Gas yield per unit solids destroyed, m <sup>3</sup> /kg (cu ft/lb)	Methane content (%)
Fat	1.2–1.6 (19–26)	62–72
Scum	0.9–1.0 (14.4–16)	70–75
Grease	1.1 (17.6)	68
Crude fibers	0.8 (12.8)	45–50
Protein	0.7 (11.2)	73
PS + WAS blend (typical)	0.8–1.1 (13–18)	60–70

Source: Design of Municipal Wastewater Treatment Plants, WEF, 2009

# Anaerobic Digestion of Biosolids



**Egg-Shaped  
Digesters**



**Conventional Digesters**



# How Can We Increase Digester Gas Production?

**Alternative Digestion or  
Biosolids Conditioning**

**FOG / Food Waste**

**Primary Treatment**





# FOG Receiving Designed by HDR



**Napa Sanitation District FOG  
Designed in 2011**



**City of Watsonville, CA  
Designed in 2002**

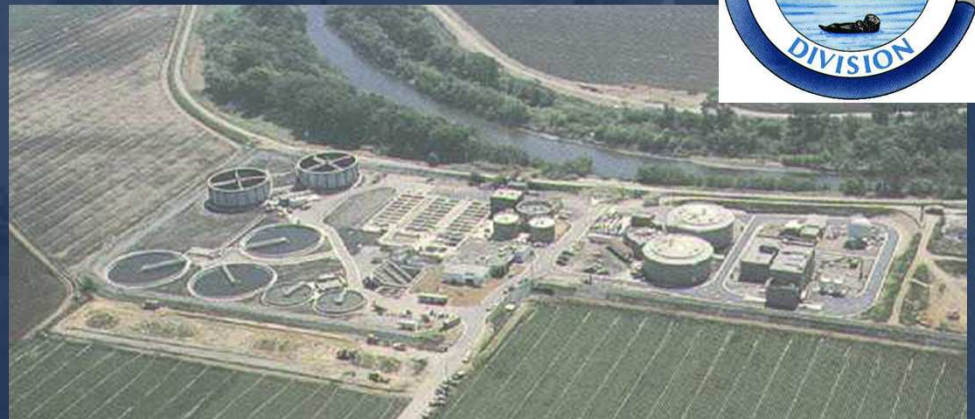
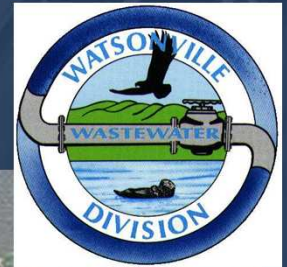


# **Case Study Watsonville, CA**

- **Produce more biogas to utilize excess digester capacity**
- **Accept grease hauler truck loads – restaurant grease traps and other sources**
- **Project on-line January 2003: Compare 2002 thru 2006 digester gas production**

# Plant Description

- Average Daily Flow
  - 12.1 mgd Design
  - 7.4 mgd for 2002
  - 7.1 mgd for 2003
- Activated Sludge
- Digesters
  - Two 90-foot-diameter, 31.5 ft SWD, 1.5 MG each, primary/secondary operation
- Cogeneration System
  - One 600 kW engine generator, dual fuel digester gas/natural gas
- Digester Gas Storage Sphere (32-foot-diameter)





# The Plan

- Feed grease to the primary digester to increase digester gas production and reduce natural gas purchases
- Cogeneration historically fueled with DG/NG
  - Fuels are blended at variable ratios, and adjusted one to two times daily
- Will grease digestion work?
  - Survey of other plants doing similar
- Watsonville has some similar experience with fruit waste digestion

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graph TD; A([Design Considerations]) --- B([Percent Grease/Water in Truck Load]); A --- C([Existing gas utilization and estimated tip fee revenue]); A --- D([Capital Cost Estimate]); A --- E([Digester Mixing]); A --- F([Grease Metering to Digester]); A --- G([Grease Holding Tank, Heating, and Mixing (Chopper Pump)]); A --- H([Location of Grease receiving station]); A --- I([Grease Conversion to Digester Gas]); A --- J([Evaluate Grease digestion capacity]); A --- K([Volume of Grease Per Day]);
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**Design Considerations**

**Percent Grease/Water in Truck Load**

**Existing gas utilization and estimated tip fee revenue**

**Capital Cost Estimate**

**Digester Mixing**

**Grease Metering to Digester**

**Grease Holding Tank, Heating, and Mixing (Chopper Pump)**

**Location of Grease receiving station**

**Grease Conversion to Digester Gas**

**Evaluate Grease digestion capacity**

**Volume of Grease Per Day**

# Design Criteria

<b>Grease Holding Tank</b>	<b>11,000-gallon tank - Two 3,000 gallon loads/day</b>
<b>Grease Holding Tank Mixing Pump</b>	<b>Chopper Pump (300 gpm)</b>
<b>Digester Mixing Pump</b>	<b>Chopper Pump (5,000 gpm)</b>
<b>Grease Metering Pump</b>	<b>PD Pump (25 gpm)</b>
<b>Grease Holding Tank Heating System</b>	<b>Hot Water Piping Inside Tank (25 gpm)</b>
<b>Odor</b>	<b>Small Activated Carbon Canister at Top Manway</b>



## **Design Criteria (continued)**

- **6,000 gpd of grease mixture based on increase in digester gas production necessary to eliminate natural gas purchases**
- **Additional volatile solids loading to digester**
- **No increase in SRT in digester**

# Grease Holding Tank & Mixing Pump



# Grease Feed Pump (25 gpm)



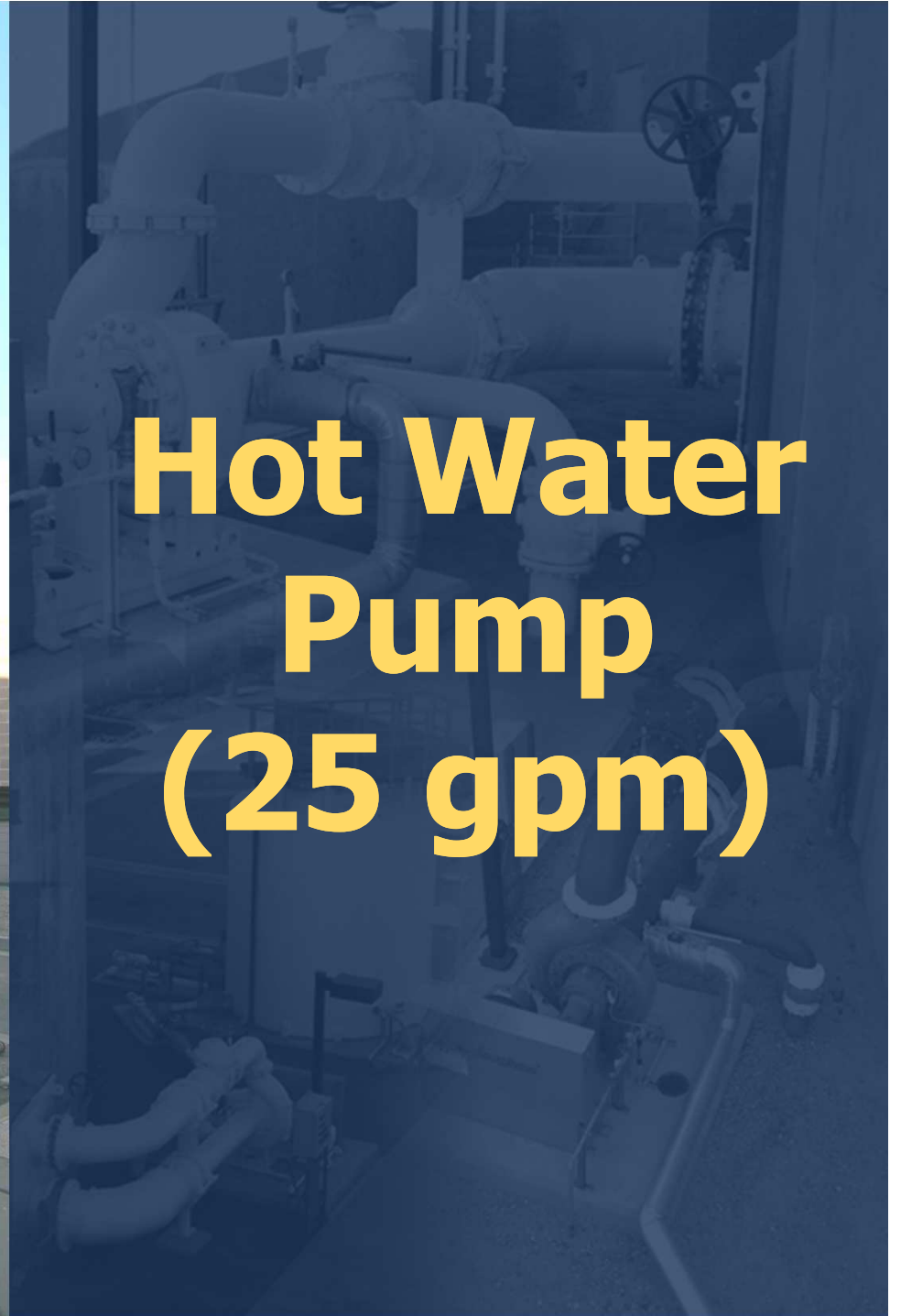


# Digester Mixing Pump (5,000 gpm)





# Hot Water Pump (25 gpm)



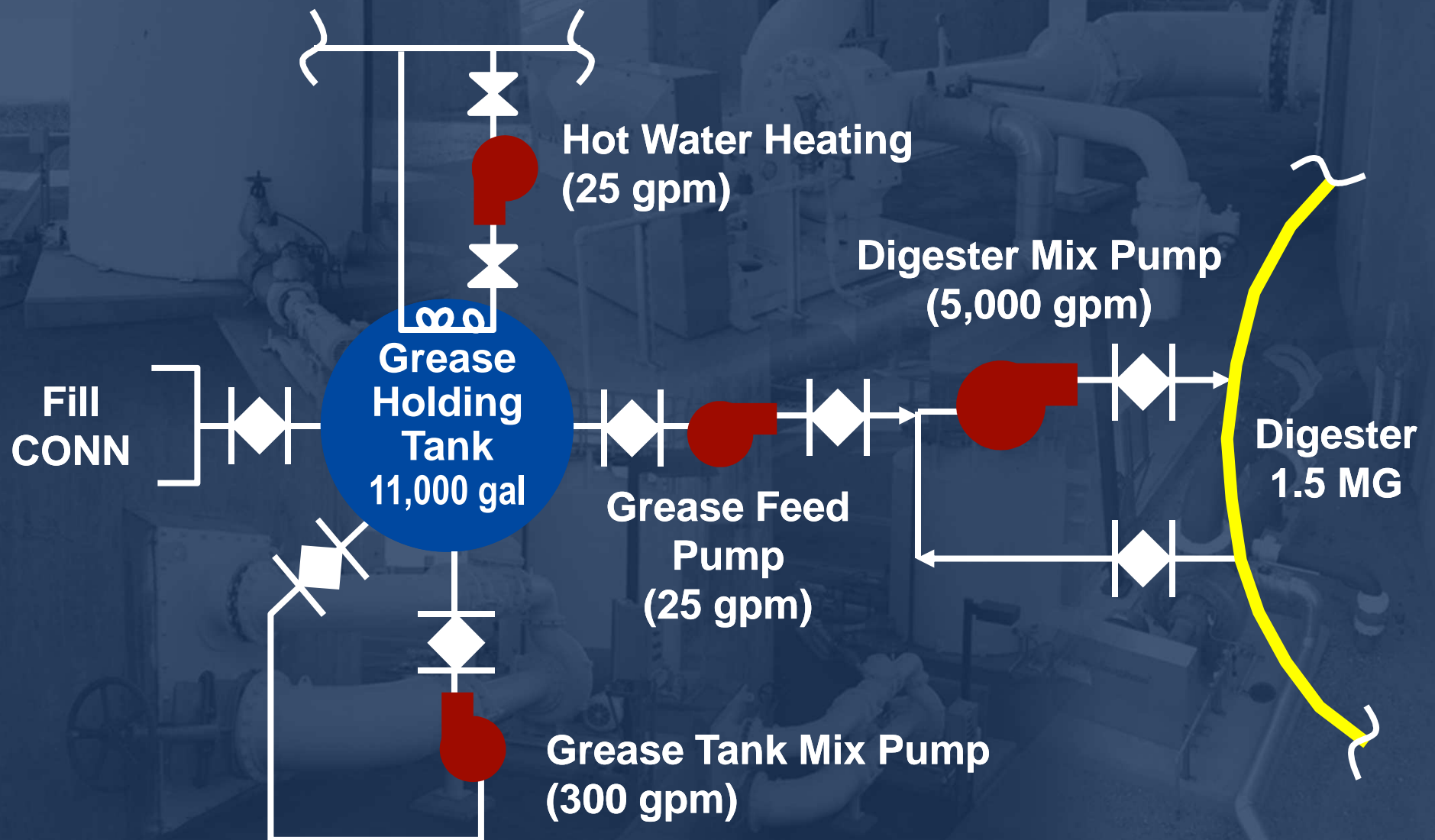


# Grease Unloading





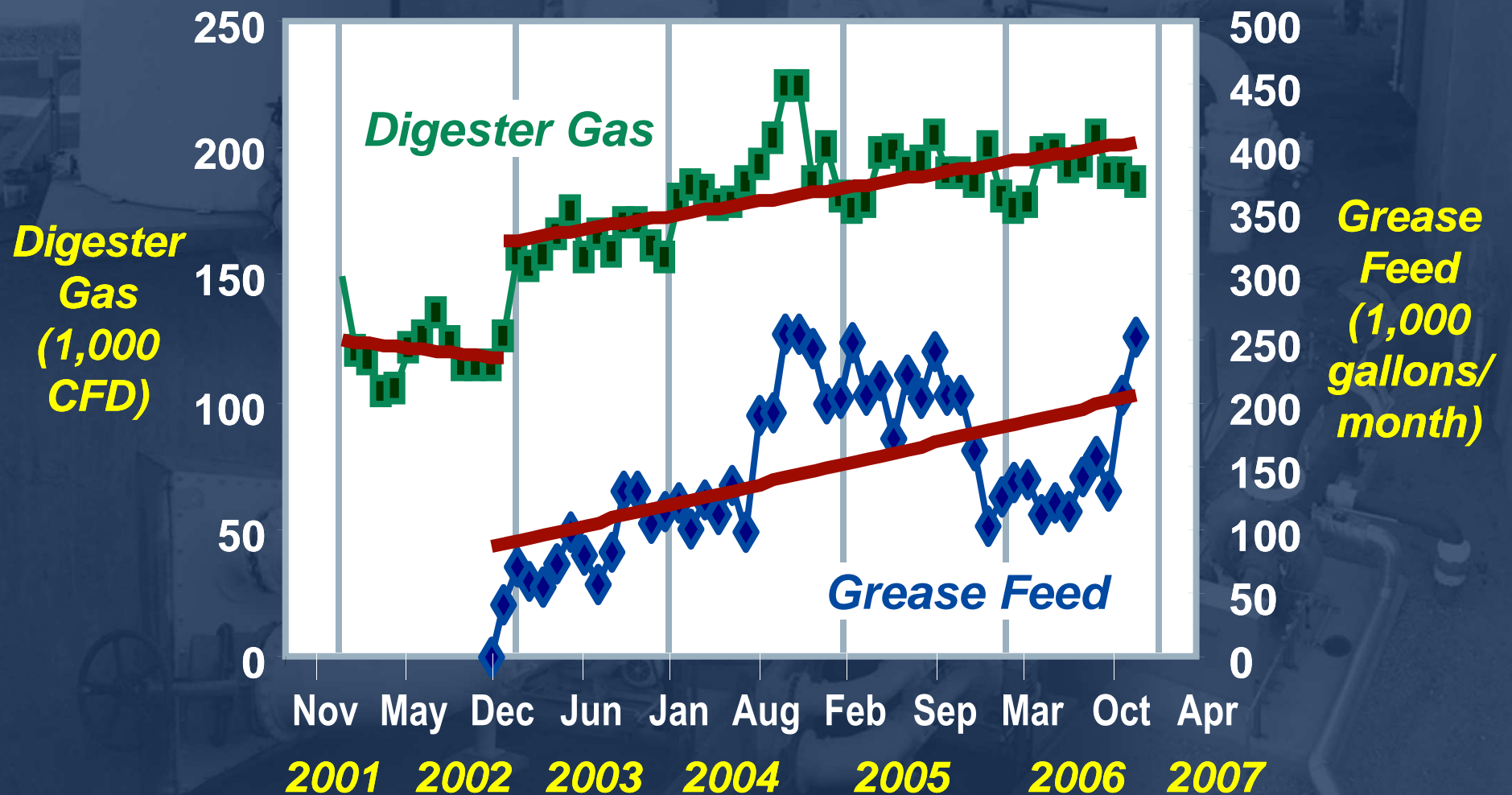
# Grease Digestion Schematic



# Project Economics

- Revenue is dependent upon natural gas avoided costs and grease tipping fees
- Maximum savings = Natural gas purchased for cogeneration plus tipping fees
- Capital cost = \$270,000 actual
- Mixing energy savings – external pump mixing vs gas mixing (minor energy savings)
- O&M savings – gas mixing compressor not in use
- Grease tipping fees - \$0.036/gallon

# Digester Gas Production vs. Grease Feed





# Results

**Startup - January 2003**

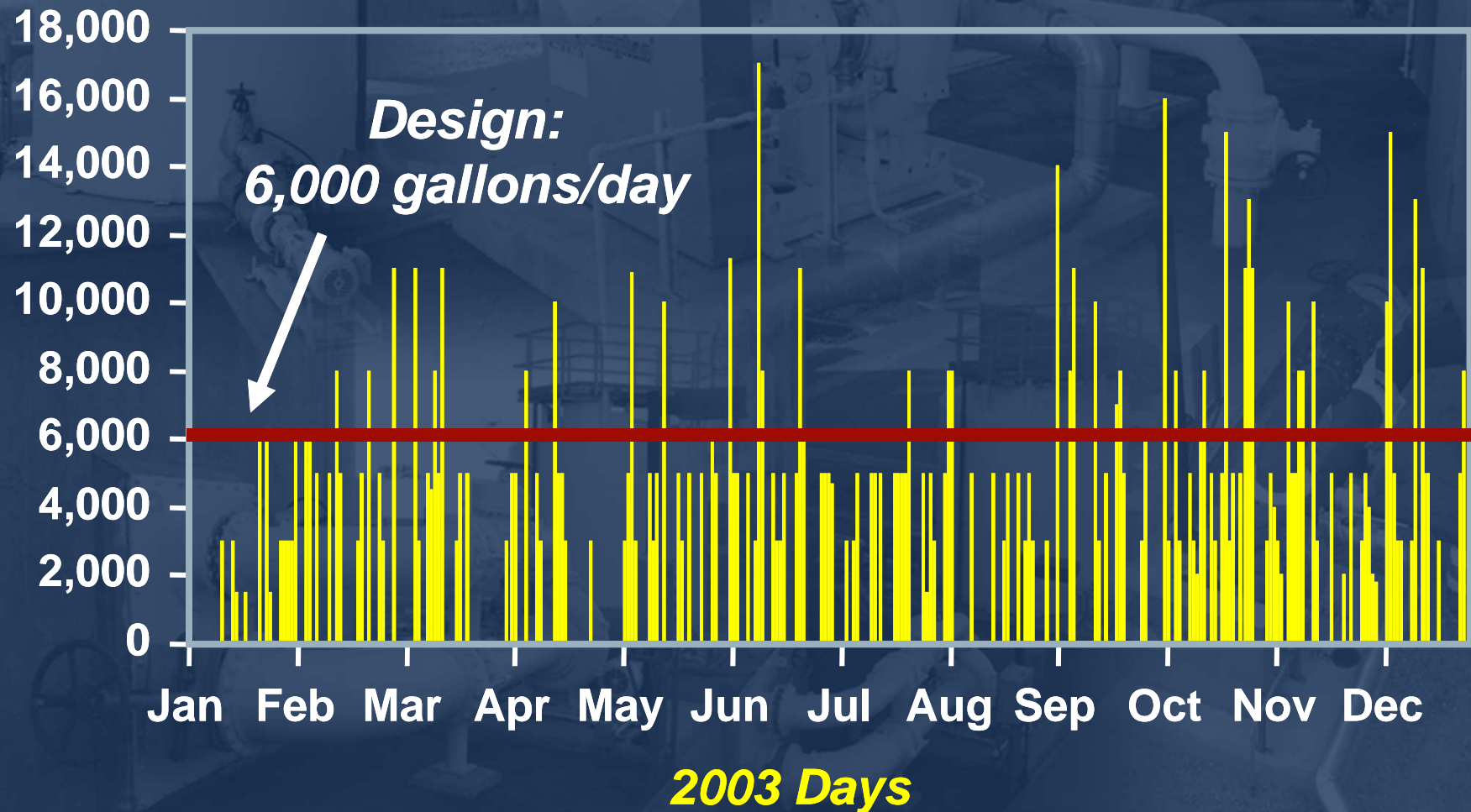
**Build it and they will come –  
if disposal fees are discounted**

**Anticipated versus actual grease received**

**No tight control on grease delivery**

# 2003 Daily Grease Loads

**Gallons**



# Grease/Water Mix

- Design assumption 40% grease
- 15% to 20% grease during first year of operation based on increased gas production
- Confirmation from other sources
- Increase acceptance from 6,000 gpd original design to 12,000-16,000 gpd
- Need to pump faster





# Grease to Power Economics

- 17% grease, 83% water
- 100% volatile solids, 100% digested
- 15 cf/lb volatile solids destroyed
- 600 btu/cf
- 32% engine-generator efficiency
- 120 KW per 3,000 gal load per day
- At \$0.10/KWH - \$288/day
- \$0.096/gal



# Summary of Grease Digestion Savings

Year	CFD NG	CFD DG	Grease Gal/Day	CFD NG Dec	CFD DG Inc	Grease Revenue	NG Savings	Total Savings
2002	98,124	113,250	0	0	0	\$0	\$0	\$0
2003	84,150	143,204	2,612	13,974	29,954	\$34,315	\$61,207	\$95,522
2004	71,250	179,998	5,232	26,874	66,747	\$68,742	\$117,708	\$186,450
2005	65,017	166,457	6,471	33,107	53,206	\$85,027	\$145,010	\$230,036
2006	68,668	185,868	4,526	29,456	72,618	\$59,473	\$129,018	\$188,491
Totals						\$247,557	\$452,943	\$700,499

# Next Time

- ❖ Intake Screen(s)
- ❖ Higher Capacity Digester Feed Pump
- ❖ Larger or second grease holding tank



# FOG Digestion Can Increase Digester Gas by 50% to 100%



- Virtually 100% volatile solids destruction
- Highly degradable
- Relatively easy to accept, process, and find
- Very small increase in biosolids production
- May improve volatile destruction of primary/WAS

# **Food Waste Co-digestion**

- **Requires excess digester capacity . Same benefits. High energy, more biogas, minimal extra solids produced, additional revenue.**
- **Food Waste can be liquid such as cheese or yogurt whey. Feed to anaerobic digester reduces load on energy intensive secondary treatment.**

# Food Waste Transfer Station Tipping Floor



**SSO food waste is 30% solid and 70% liquid.  
Will require desizing and depackaging  
(Grinding/pulping)**



## **Foodwaste Co-Digestion at WWTF in New York**

- **Two anaerobic digesters at municipal treatment facility with low industrial load**
- **Solution: Co-digestion - Adding primary solids and dairy wastes, e.g. yogurt and cheese whey from local manufacturers.**
- **Since 2002 after several upgrades to plant, Gloversville Johnstown WWTP have double VS load and electricity output.**
- **CHP generating nearly all the electric power for the municipal WWTP plant.**

# FOG and Foodwaste

🇺🇸 Thank You

🇺🇸 QUESTIONS????

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